

Comparison Analysis and Calculation Of Cooling Capacity Of GTU Inlet Air A Cooling Systems For Climatic Conditions With Saving Fuel Cost For Three Regions Of Libayn Jalu, Hon , Tripoli

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ABSTRACT: Gas turbine (GT) generators are the base of electricity branch in Libya. Gas turbine performance in Libya are characterized by high intake air temperatures and their fuel efficiency falling as a result that requires the intake air cooling. Absorption lithium-bromide chillers providing a gas turbine intake air temperature decrease down to 15 °C and absorption aqua-ammonia and refrigerant ejector chillers with air temperature decrease down to 10 °C and lower using the heat of turbine exhaust gas are discussed as waste heat thermo transformers. A fuel saving due to cooling of the air at the inlet of gas turbines down to varies temperatures by thermo transformers of different types has been evaluated for regions of Libya where electricity production in turbo generators is concentrated. It was shown that gas turbine intake air cooling down to the temperatures of 10 absorption aqua-ammonia and refrigerant ejector chillers provides annular fuel saving (1.5) times larger as compared with absorption lithium-bromide chillers providing a gas turbine intake air temperature decrease down to 15 °C. The higher efficiency of gas turbine intake air deep cooling down to the temperatures of 10 and absorption aqua-ammonia and refrigerant ejector chillers has been proved as a result. The annular fuel saving due to air cooling at the inlet of gas turbine generators by thermo transformers of different types has been evaluated for 3 regions of Libya where the electricity production ,Taking into account daily and seasonal changes in climatic conditions, and the cooling capacity allocated to air cooling.

Key words: gas turbine generator, fuel saving, absorption lithium-bromide chiller, refrigerant ejector chiller, absorption aqua-ammonia chiller, intake air cooling, exhaust gas waste heat recovery, climatic conditions.

1.INTRODUCTION.

Gas turbine(GT) generators are the base of electric power sector of Libya .The electricity production is concentrated in six regions: Tripoli (32 %), Benghazi (15 %), West Region (20 %), Middle Region (18%), East Region (6%), South Region (9%) [1]. Efficiency of gas turbines (GT) significantly depends on ambient air temperature t_{amb} at the inlet and sharply decreases with its increase [1–2]. So, the air temperature increase at the inlet of General Electric GT LM2500+ (Ne = 27 MW at $t_{amb} = 15$ °C) on 10 °C causes decrease in GT efficiency by 2% with corresponding increase in specific fuel consumption b_e , and for GT LM1600(Ne = 15 MW) – approximately by 1.6% [1]. Because of the intake air temperature raising the electrical power output of GT are by 15–20% lower than nominal value at $t_{amb} = 15$ °C [2]. Therefore the problem of GT intake air cooling is particularly actual in energetic of Libya A deficit of fresh water makes difficult the application of

evaporative cooling of GT intake air [2] in the regions of Libya with arid hot climate where the effect from inlet fogging could be very essential. In such conditions pre-cooling GT intake air by waste heat recovery chillers (WHRC) utilizing exhaust gas heat can be a real alternative. As a working fluid an ammonia and water boiling under vacuum are used for aqua-ammonia chiller (AAC) and absorption lithium-bromide chiller (ABC) respectively and ozone-safe refrigerants R142B and R600 for refrigerant ejector chillers (REC) [3–4]. As ambient air parameters are characterized not only seasonal, but also daily fluctuations of temperature t_{amb} and relative humidity ϕ , it is necessary to solve a problem of choice of the specified (designed) refrigeration capacity of WHRC which, on one hand, has to provide whenever possible maximum decrease in GT intake air temperature and, respectively, maximum fuel saving, and on the other hand, minimizing operation of WHRC at lowered refrigeration capacity and, therefore, not proved increased capital expenditure for WHRC, ammonia in absorption aqua-ammonia thermo transformer (REC) the gas turbine intake air can be chilled to the temperature $t_{a2} = 10$ °C and even down to 7 °C (with $t_x = 2...3$ °C) [1, 7], but in the case of water applied as a coolant in absorption lithium-bromide thermo transformers (ABC) the temperature of chilled air is higher: $t_{a2} = 15...17$ °C ($t_x \approx 7$ °C) [7,8,9, 10].

goal of the analysis the efficiency of GT intake air cooling of designed refrigeration capacity of WHRC providing maximum fuel saving due to cooling of air according to climatic conditions of operation.

2. RESULTS OF INVESTIGATION.

As mentioned above the performance conditions of GT are characterized by daily fluctuations of intake ambient air temperature t_{amb} and relative humidity ϕ that influences thermodynamic efficiency of GT and, respectively, specific fuel consumption b_e [1–2]. Changes in ambient air parameters within July 2009 for Tripoli and Hon and Jalu (the southern region of Libya with arid tropical climate) are presented in Figure 1.

Apparently, daily considerable fluctuations of ambient air temperature t_{amb} of 10–15 °C and relative humidity ϕ are characterized by existence of day and night opposite directed maximum and minimum values of t_{amb} and ϕ : to maxima of temperatures t_{amb} correspond minima of humidity ϕ in the afternoon and vice versa at night. Their existence creates favorable conditions for bigger decrease in GT intake air temperature in the afternoon when considerable reduction of thermodynamic efficiency of GT takes place

caused by the raised temperatures t_{amb} , but corresponding lowered humidity ϕ causes some decrease in thermal load on WHRC.

Depth of air cooling in the heat exchanger is defined by temperature of a coolant and intensity of heat transfer. So, at the intensive heat exchange providing the minimum difference of temperatures between the cooled air and a coolant (5–8 °C), cooling of air down to the temperature about 15 °C in the air cooler by water (AC) of the absorption lithium bromide chiller (ABC) and to 10 °C in the refrigerant evaporator-air cooler (E-AC) of the refrigerant ejector chiller (REC) is possible. Schemes of cooling systems of GT intake air in ABC and REC with utilization of exhaust gas heat are given in Figure 2.

The WHRC consists of high-temperature (waste heat utilization) and low-temperature (refrigeration) contours. So, in the high-temperature contour of ABC the heat of GT exhaust gas is used for evaporation of water from water lithium-bromide mixture in the generator-desorbed GD (Figure 2(a)) with next condensation of water vapour by extracting its heat into surroundings in cooling tower. In the low-temperature contour the water is evaporated under vacuum with extracting the heat of evaporation from another water as a coolant and thus producing refrigeration capacity spent for GT intake air cooling.

pressure refrigerant vapour as a motive fluid for ejector Ej to compress the low pressure refrigerant vapour (at refrigerant boiling temperature $t_0 = 2-5$ °C), sucked from refrigerant evaporator-air cooler E-AC of refrigeration contour with increasing its pressure up to the pressure in the condenser Con (at refrigerant condensing temperature t_c).

The air temperature decrease $\Delta t = t_{amb} - t_{a2}$ and, respectively, the gained effect of GT intake air cooling depends on the current ambient air temperature t_{omb} and air cooled temperature t_{a2} which, in its turn, depends on the temperature of a coolant – cold water t_{cw} or boiling refrigerant t_0 , i.e. on the type of WHRC: in ABC the air could be cooled to $t_{a2} = 15-20$ °C (cold water $t_{cw} = 7-10$ °C), but in REC – to lower temperature $t_{a2} = 7-10$ °C (boiling refrigerant $t_0 = 2-4$ °C) [4].

Values of decrease in air temperature Δt_{15} when cooling GT intake air from the current ambient temperature t_{omb} to temperature $t_{a2} = 15$ °C in ABC and values Δt_{10} for $t_{a2} = 10$ °C for cooling GT intake air in REC within July 2009 for (Tripoli) and center (Hon) and South (Jalu) are presented in Figure 3. With decrease of GT intake air cooled temperature t_{a2} in REC not only the temperature differences Δt_{10} increase (as compared with Δt_{15} in ABC), but also duration of GT operation at the lowered temperature, and consequently, total effect from cooling.

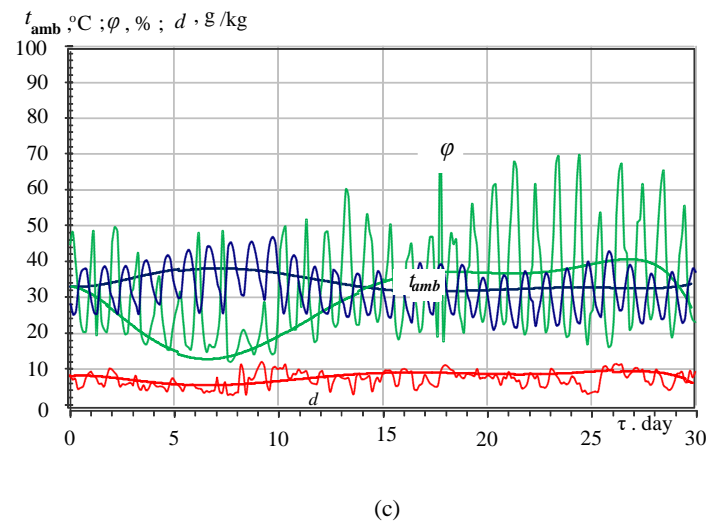
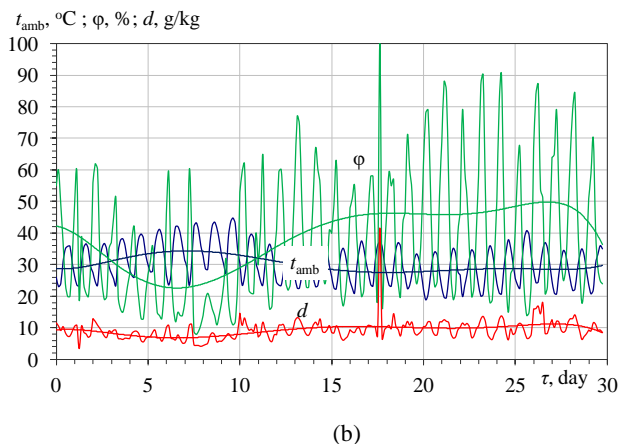
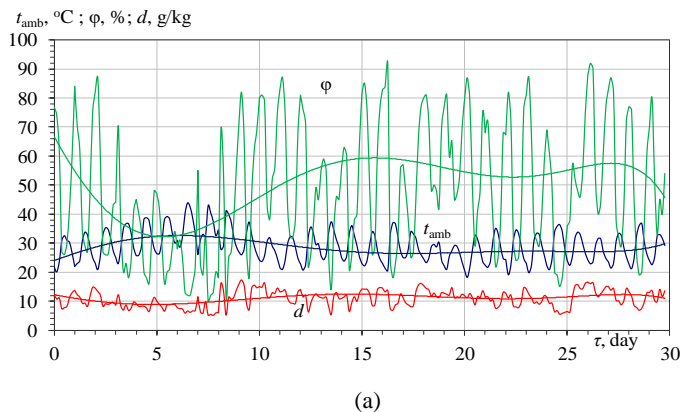


Fig.1. Change of temperature t_{amb} , relative humidity ϕ and absolute humidity d of ambient air within July, 2009 : (a) – Tripoli ; (b) – Hon ; (c) – Jalu

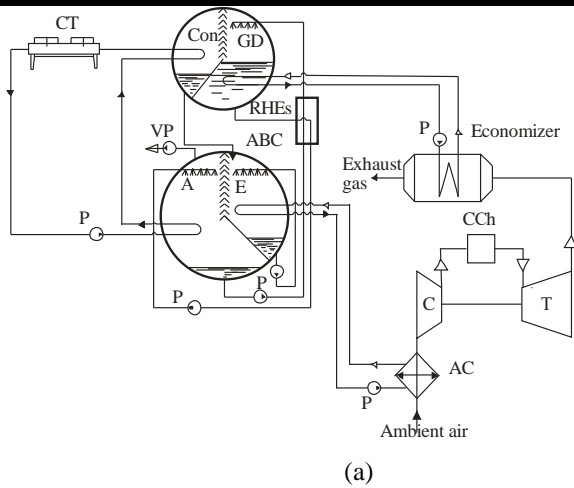


Fig. 2. Schemes of cooling systems of GT intake air in ABC (a) and REC (b) with utilization of exhaust gas heat: C – compressor; T – turbine; C C h – combustion chamber; Economizer – a water-heating utilization boiler; P – pump; ABC: GD – generator-desorber of water vapour; Con – condenser; A – absorber; E – evaporator; RHEs – regenerative heat exchanger of solutions, VP – vacuum pump; REC: E j – ejector; G – generator of refrigerant vapour; Con – condenser; E-AC – evaporator-air cooler; EV – expansion valve; CT – cooling tower.

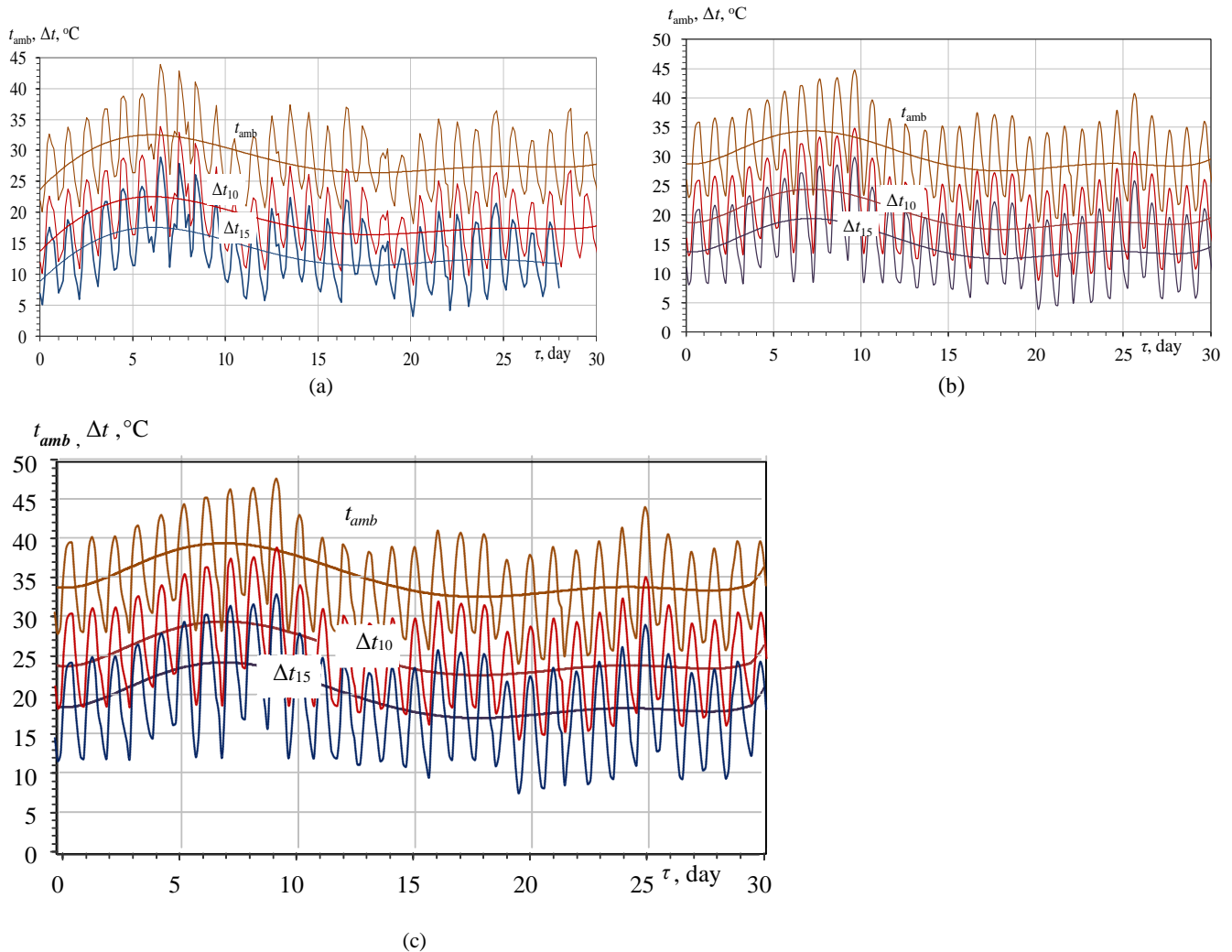
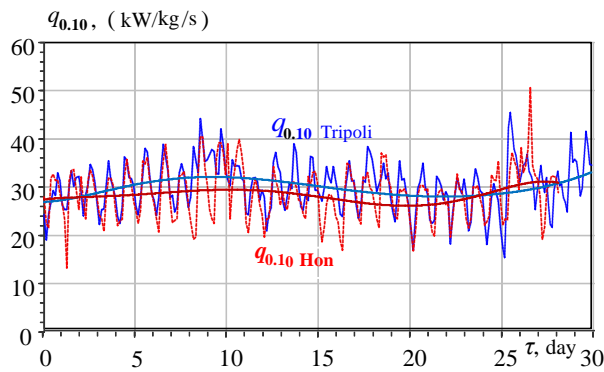


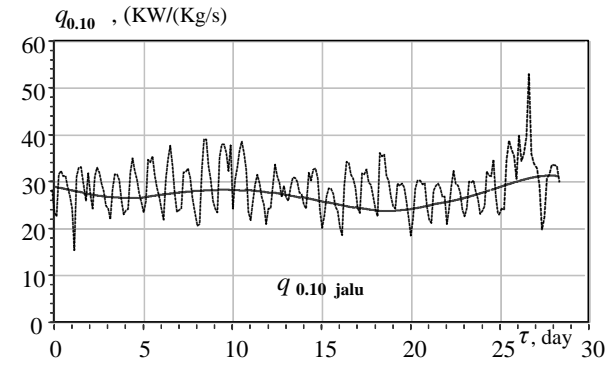
Fig. 3. Values of decrease in air temperature Δt_{15} when cooling GT intake air from the current ambient temperature t_{amb} to temperature $t_{a2} = 15^\circ\text{C}$ (in ABC) and Δt_{10} for $t_{a2} = 10^\circ\text{C}$ (in REC) within July 2009 for Tripoli (a) and Hon (b) and Jalu (c).

The refrigeration capacity Q_0 spent for GT intake air cooling depends not only on the value of temperature decrease $\Delta t = t_{amb} - t_{a2}$, i.e. on the sensible heat which is taken away from ambient air, but also on the heat of condensation of water vapor from damp air when decreasing its temperature below wet bulb temperature t_{wb} . It is more convenient to present the required refrigeration capacities of thermo transformers in the form of the specific refrigeration capacities relating on a single consumption of air $G_a = 1 \text{ kg/s}$: $q_0 = \xi \cdot c_{wa} \cdot (t_{amb} - t_{a2})$, kW/(kg/s) or kJ/kg, proceeding from which it is possible to calculate easily full established refrigeration capacity $Q_0 = q_0 \cdot G_a$ for GT consumption of air G_a , where $c_{wa} - a$

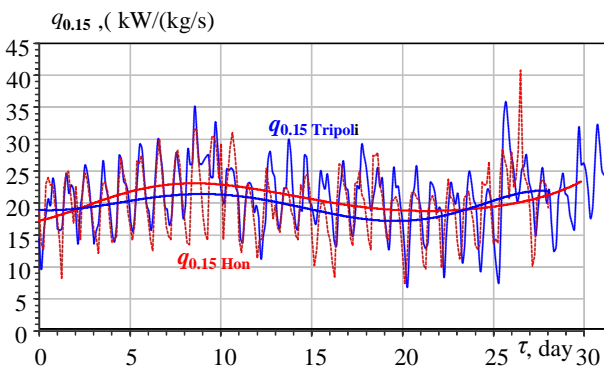
thermal capacity of damp air; ξ – total-to-sensible air heat decrease relation (total heat decrease of air related to sensible heat decrease or inversely proportional value of sensible heat rate) calculated as ratio of total heat extracted from the wet air during cooling (an air enthalpy decrease including the heat of water vapor condensation) and sensible heat extracted depending on temperature difference of air on dry thermometer $\Delta t = t_{amb} - t_{a2}$. Current values of specific refrigeration capacity q_0 for Tripoli and for Hon and for jalu when cooling GT intake air from temperature of ambient air t_{amb} to $t_{a2} = 10^\circ\text{C}$ in REC and to $t_{a2} = 15^\circ\text{C}$ in ABC in July 2009 are shown in Figure 4.



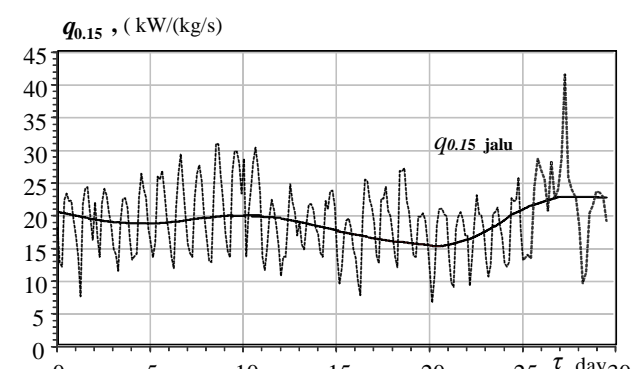
(a)



(b)



(c)



(d)

Fig. 4. Current values of specific refrigeration capacity q_0 for Tripoli and for Hon and for jalu when cooling GT intake air from ambient air temperature t_{amb} air to temperature $t_{a2} = 10^\circ\text{C}$ in REC (a,b) and $t_{a2} = 15^\circ\text{C}$ in ABC (c,d) in July 2009: (— Tripoli ; — Hon ; — jalu).

For GT with the same impact of intake air temperature depression Δt on the fuel efficiency, i.e the same decrease in specific fuel consumption Δb_e for 1°C depression of intake air temperature: $\Delta b_{e1^\circ\text{C}} = \Delta b_e / \Delta t$, it is quite convenient to use as parameter the specific fuel consumption saving – for 1 kW of GT electric power output: $B_{F,y1} = B_F / N_e$, kg/kW, where B_F – the total fuel consumption saving for GT with electric power output N_e , kW, for any time interval τ ; for the estimation of annual specific fuel consumption saving as $B_{F,y1} = \Sigma[(\Delta t \tau)] \cdot (\Delta b_e / \Delta t)$, where τ – a time interval, within which the temperature depression Δt could be assumed as constant: $\tau = 1$ h [4,6].

Dependence of GT specific electric power output for 1 kW, an annual fuel economy of $B_{F,y1} = B_F / N_e$, the kg/kw, gained as $B_{F,y1} = \Sigma[(\Delta t_b \tau)] \cdot (\Delta b_e / \Delta t)$, is resulted on fig. 5. Thus recognized that at decrease in temperature of air on an entry on 1°C a specific fuel rate decreases for magnitude $\Delta b_{e1^\circ\text{C}} = \Delta b_e / \Delta t = 0,35$ g/(kW·h).

To estimate the impact of cooling technologies considered the annual specific fuel consumption savings $B_{F,y1}$ (related to 1 kW of GT electric power output) due to GT intake air cooling from actual changing ambient temperature t_a to various cooled air temperature t_{a2} by thermo transformers of different types have been calculated for ambient conditions at the location for 3 regions of Libya (Tripoli ,Hon, Jalu) during 2009. The results of this analysis are presented in Fig.5. With this a specific fuel consumption reduction of 0.35 g/(kW·h) for every 1°C drop in gas turbine intake air temperature has been considered [1, 2].

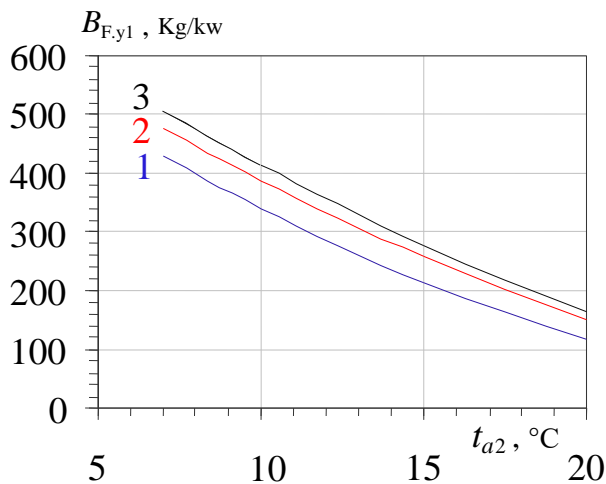


Fig. 5. Annual specific fuel consumption saving $B_{F,y1}$ (related to 1 kW of GT electric power output) due to GT intake air cooling from actual ambient temperature t_a to various cooled air temperature t_{a2} by thermo transformers of different types: $t_{a2} = 7-10^\circ\text{C}$ in RETT and AATT; $t_{a2} = 15-20^\circ\text{C}$ in ALBTT for 3 regions of Libya (— Tripoli, — Hon, — Jalu 2009).

Knowing the annual specific fuel consumption saving $B_{F,y1}$ (related to 1 kW of GT electric power output) due to GT intake air cooling, the total annual fuel consumption saving B_F for GT of any electric power output N_e may be calculated easily as $B_F = B_{F,y1} N_e$. The results of the

impact of cooling technologies considered on the total annual fuel consumption saving B_F for GT of electric power output $N_e = 10$ MW.

Annual fuel saving value of $B_{F,10\text{MW},T}$, due to cooling the air at the gas turbine inlet with an electric power of 10MW, depending on the corresponding costs of cooling power $Q_{0,10\text{MW}} = q_0 \cdot G_{a,10\text{MW}}$ at different final temperatures of cooled air t_{a2} (Tripoli, Hon, Jalu 2009) $B_{F,10\text{MW},T}$ at $t_{a2} = 10; 15$ and 20°C are presented in Fig.6. at the same time, it was believed that for a gas turbine unit with an electric power of 10 MW the air flow rate $G_{a,10\text{MW}} = 40$ kg/s (taken by analogy with LM1600) [2], based on which the cost of refrigeration power for air cooling with a flow rate of $G_{a,10\text{MW}} = 40$ kg/s was calculated as $Q_{0,10\text{MW}} = q_0 \cdot G_{a,10\text{MW}} = \xi \cdot c_{wa} \cdot (t_{amb} - t_{a2}) \cdot G_{a,10\text{MW}}$, Kw.

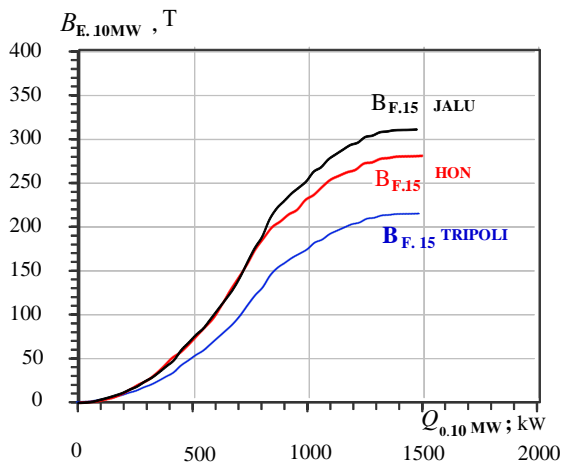
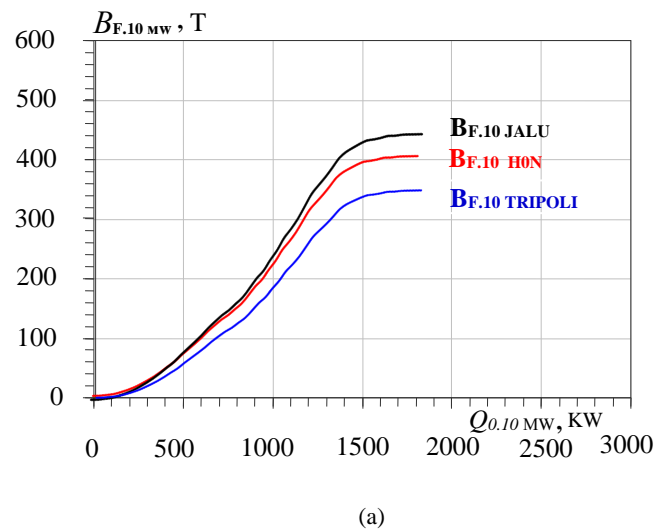


Fig.6. values of the annual specific fuel saving $B_{F,10\text{MW},T}$, due to cooling at the gas turbine inlet with an electric power of 10 MW depending on the corresponding costs of cooling power $Q_{0,10\text{MW}}$, Kw, at different final temperatures of cooled air t_{a2} (— Tripoli; — Hon; — jalu, 2009): $B_{F,10}$ at $t_{a2} = 10^\circ\text{C}$ in REC (a) and t_{a2} (— Tripoli; — Hon; — jalu, 2009): $B_{F,15}$ at $t_{a2} = 15^\circ\text{C}$ in ABC (b).

From Fig.6.(a). Apparently, for climatic conditions of Tripoli when cooling GT intake air to the temperature $t_{a2} = 10^\circ\text{C}$ the refrigeration capacity of REC $Q_{0.10\text{MW}} = 1520$ kW provides the value of annual specific fuel saving $B_{F10} = 340$ T at high rates of its increment. The further increase in refrigeration capacity above $Q_{0.10\text{MW}} = 1520$ kW does not lead to any noticeable increase in fuel saving $B_{F.10}$. Thus, proceeding from the refrigeration capacity $Q_{0.10\text{MW}} = 1520$ kW the full designed refrigeration capacity of REC can be adopted for climatic conditions of Tripoli: $Q_{0.10\text{MW}} = q_0 \cdot G_a$, kW. A little less value of rational specific refrigeration capacity $Q_{0.10\text{MW}} = 1440$ kW can be adopted for climatic conditions of Hon, that provides value of annual specific annual specific fuel saving $B_{F.10} = 390$ T, i.e. increased by 15% as compared with Tripoli. A slightly lower value of specific cooling capacity $Q_{0.10\text{MW}} = 1400$ kW can also be adopted for the climatic conditions of Jalu, providing an annual specific fuel saving value $B_{F.10} = 410$ T, i.e., a 5% increase compared to Hon and 20% increase compared to Tripoli due to the larger value of the inlet air temperature drop GT Δt from higher ambient air temperatures t_{amb} .

From Fig.6. (a).

Accordance with Fig.6.(a) of (Tripoli), When cooling the air at the gas turbine inlet with an electric power of 10 MW in REC (up to a temperature $t_{a2} = 10^\circ\text{C}$), the rational installed cooling power $Q_{0.10\text{MW}} = 1520$ kW, which provides annual fuel saving $B_{F.10} = 340$ T, or $340 \text{ T} / 0.8 \cdot 10^{-3} \text{ T/M}^3 = 425$ thousand. M^3 , which at a cost of 500 \$/thousand. M^3 is 213 thousand. \$/year, annual income $I_{\text{REC}} = 213$ thousand. \$ for electric gas turbine unit 10 MW, for climatic conditions of (Hon) When cooling the air at the gas turbine inlet with an electric power of 10 MW in REC (up to a temperature $t_{a2} = 10^\circ\text{C}$), the rational installed cooling power $Q_{0.10\text{MW}} = 1440$ kW, which provides annual fuel saving $B_{F.10} = 390$ T, or $390 \text{ T} / 0.8 \cdot 10^{-3} \text{ T/M}^3 = 488$ thousand. M^3 , which at a cost of 500 \$/thousand. M^3 is 244 thousand. \$/year, annual income $I_{\text{REC}} = 244$ thousand. \$ for electric gas turbine unit 10 MW, of (Jalu) When cooling the air at the gas turbine inlet with an electric power of 10 MW in REC (up to a temperature $t_{a2} = 10^\circ\text{C}$), the rational installed cooling power $Q_{0.10\text{MW}} = 1400$ kW, which provides annual fuel saving $B_{F.10} = 410$ T, or $410 \text{ T} / 0.8 \cdot 10^{-3} \text{ T/M}^3 = 513$ thousand. M^3 , which at a cost of 500 \$/thousand. M^3 is 257 thousand. \$/year, annual income $I_{\text{REC}} = 257$ thousand. \$ for electric gas turbine unit 10 MW.

From Fig.6. (b). climatic conditions of Tripoli when cooling GT intake air to the temperature $t_{a2} = 15^\circ\text{C}$ the refrigeration capacity of REC $Q_{0.10\text{MW}} = 1240$ kW provides the value of annual specific fuel saving $B_{F15} = 210$ T at high rates of its increment. The further increase in refrigeration capacity above $Q_{0.10\text{MW}} = 1240$ kW does not lead to any noticeable increase in fuel saving $B_{F.15}$. Thus, proceeding from the refrigeration capacity $Q_{0.10\text{MW}} = 1240$ kW the full designed refrigeration capacity of REC can be adopted for climatic conditions of Tripoli: $Q_{0.10\text{MW}} = q_0 \cdot G_a$, kW. A little less value of rational

specific refrigeration capacity $Q_{0.10\text{MW}} = 1160$ kW can be adopted for climatic conditions of Hon, that provides value of annual specific annual specific fuel saving $B_{F.15} = 260$ T, i.e. increased by 23% as compared with Tripoli. A slightly lower value of specific cooling capacity $Q_{0.10\text{MW}} = 1120$ kW can also be adopted for the climatic conditions of Jalu, providing an annual specific fuel saving value $B_{F.15} = 280$ T, i.e., a 7% increase compared to Hon and 33% increase compared to Tripoli due to the larger value of the inlet air temperature drop GT Δt from higher ambient air temperatures t_{amb} .

From fig .6. (b), Of (Tripoli), In the case of cooling at the inlet of the gas turbine unit in the ABC ($t_{a2} = 15^\circ\text{C}$), the fuel saving $B_{F15} = 210$ T, for which it is necessary to use the ABC with an installed refrigeration capacity $Q_{0.10\text{MW}} = 1240$ kW. Then the annual income $I_{\text{ABC}} = 131$ thousand. \$ for a gas turbine unit with an electrical capacity of 10 MW, Of (Hon) In the case of cooling at the inlet of the gas turbine unit in the ABC ($t_{a2} = 15^\circ\text{C}$), the fuel saving $B_{F.15} = 260$ T, for which it is necessary to use the ABC with an installed refrigeration capacity $Q_{0.10\text{MW}} = 1160$ kW. Then the annual income $I_{\text{ABC}} = 163$ thousand. \$ for a gas turbine unit with an electrical capacity of 10 MW, Of (Jalu) In the case of cooling at the inlet of the gas turbine unit in the ABC ($t_{a2} = 15^\circ\text{C}$), the fuel saving $B_{F.15} = 280$ T, for which it is necessary to use the ABC with an installed refrigeration capacity $Q_{0.10\text{MW}} = 1120$ kW. Then the annual income $I_{\text{ABC}} = 175$ thousand. \$ for a gas turbine unit with an electrical capacity of 10 MW.

Fig .7. Show diagram of the potentially possible effect of cooling the air at the inlet of the GTU in terms of fuel savings B_F and increased electricity production $\Sigma(\Delta N_{\text{e}\Sigma} \cdot \tau)$, taking into account the capacities of electric generating GTU and the climatic conditions of 3 regions of Libya 1- Tripoli ; 2- center (Hon) ; 3- south (Jalu).

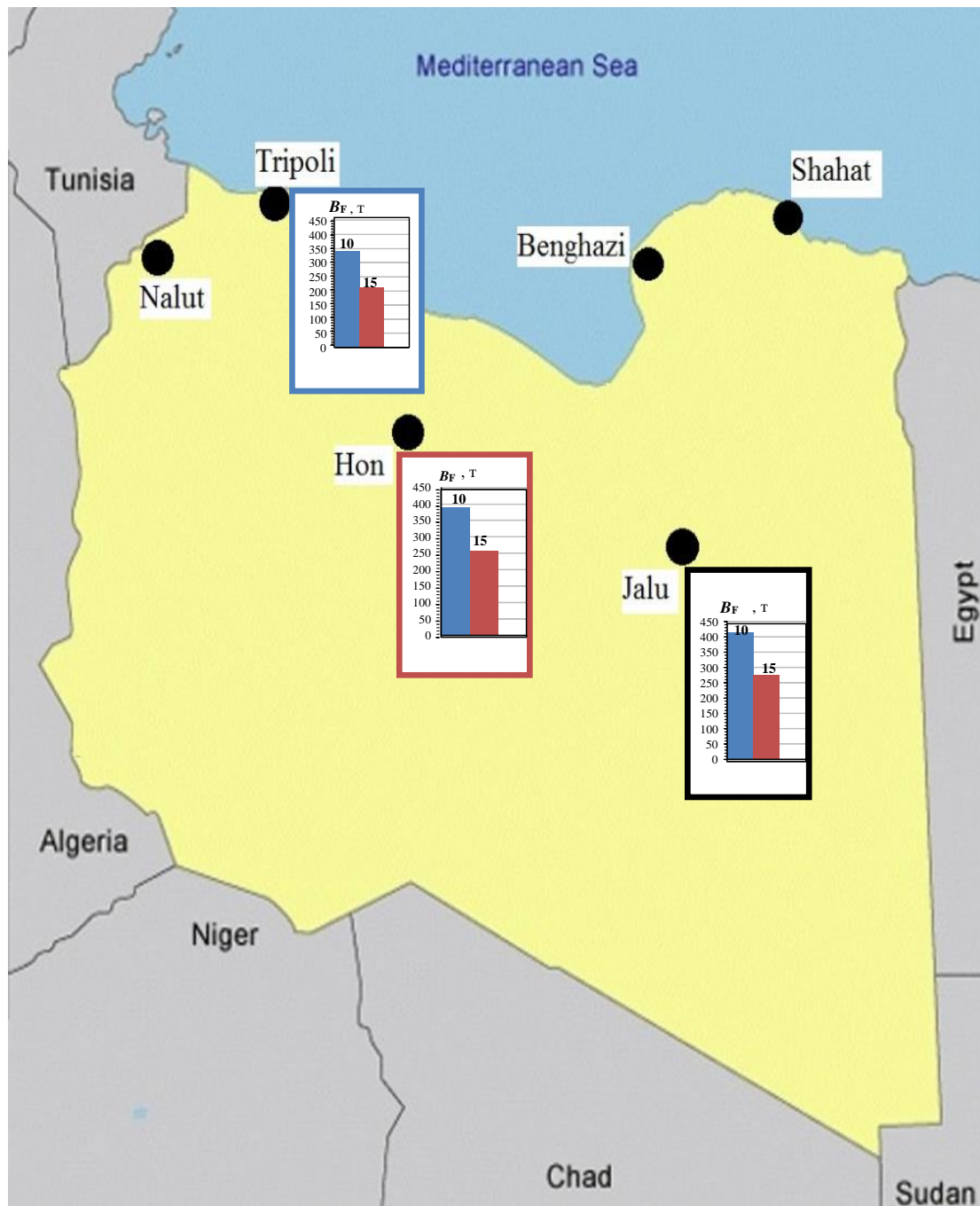


Fig.7. Values of annual fuel savings in BF due to air cooling at the gas turbine inlet from the current temperature t_a to $t_{a2} = 10^\circ\text{C}$ (in REC) , $t_{a2} = 15^\circ\text{C}$ (in ABC) , for gas turbines of power plants in 3 regions: 1 – Tripoli ; 2 - Center (Hon) ; 3 - South (Jalu).

3.CONCLUSIONS.

On the basis of the analysis of potentially possible decrease in temperature of GT intake air due to its cooling in WHRC by utilizing the exhaust gas heat the corresponding fuel savings are defined. The ABC and REC as WHRC providing cooling of GT intake air respectively to 15 °C and 10 °C are considered. We found that the rationally designed cooling capacity of the WHRC provides the maximum cooling effect through annual fuel savings, as deep cooling of the GT inlet air to a temperature of $t_{a2} = 10^{\circ}\text{C}$ in the REC saves (1.5) times the annual fuel economy cost compared to cooling the air to a temperature of $t_{a2} = 15^{\circ}\text{C}$ in the ABC. The effect of air cooling on the GTU inlet was estimated in the form of annual fuel savings in 3 regions of Libya where the electricity industry is concentrated by gas turbine power plants, taking into account daily and seasonal variations in ambient air temperature and relative humidity.

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